- 1 1. A hydrocarbon mixture comprising:
- 2 an olefin/paraffin mixture having a carbon number range from about C<sub>8</sub> to about C<sub>20+</sub>
- 3 wherein the olefin/paraffin mixture comprises:
- 4 substantially no oxygenates;
- between about 1 wt% and 20 wt% olefin wherein at least about 1 wt% of the olefin is mono-olefin;
- 7 at least about 5 wt% n-paraffins;
- between about 2 and 94 wt% branched paraffins wherein at least about 30% of
  all branch groups are monomethyl and wherein the ratio of terminal monomethyl
  branching to internal monomethyl branching is at least about 1:1.5.
- 1 2. The hydrocarbon mixture of claim 1 wherein the ratio of terminal monomethyl branching to internal monomethyl branching is at least about 1:1.
- 1 3. The hydrocarbon mixture of claim 1 wherein the n-paraffins are present in an amount of at
- least about 10 wt% and wherein the ratio of terminal monomethyl branching to internal
- monomethyl branching is at least about 1.5:1.
- 1 4. The hydrocarbon mixture of claim 1 wherein the n-paraffins are present in an amount of at
- least about 10 wt% and wherein the ratio of terminal monomethyl branching to internal
- monomethyl is at least about 2:1.
- 1 5. The hydrocarbon mixture of claim 1 wherein the olefin/paraffin mixture is a product of a
- 2 Fischer-Tropsch reaction.
- 1 6. The synthetic fuel of claim 5 wherein the Fischer-Tropsch reaction feed syngas comprises
- 2 10-65% N<sub>2</sub>.
- 1 7. A process for producing a synthetic fuel comprising the steps of:

producing a light Fischer-Tropsch liquid; 2 (a) dehydrating all or a part of the FT oxygenates in the LFTL while retaining the 3 (b) olefin content in the LFTL; 4 recovering an organic phase from the product of step (b); 5 (c) blending the organic phase into a transportation fuel. 6 (d) 8. The process of claim 7 further comprising the step of (a<sub>1</sub>) vaporizing the LFTL before step 1 (b) and after step (a). 2 9. The process of claim 8 wherein the dehydrated product from step (b) is in the gaseous state 1 and step (c) further includes condensing the dehydrated product. 2 10. The process of claim 9 wherein the heat from condensing the dehydrated product is 1 recycled to at least partially vaporize the LFTL in step (a1). 2 11. The process of claim 7 wherein the light Fischer-Tropsch liquid is produced from a feed 1 syngas having 10-65% N<sub>2</sub>. 2 12. The process of claim 11 wherein the feed syngas is produced by autothermal reformation in the presence of air. 13. A hydrocarbon mixture comprising: 1 a paraffin mixture having a carbon number range from about  $C_8$  to about  $C_{20^+}$  wherein 2 the paraffin mixture comprises: 3

substantially no FT oxygenates;

at least about 5 wt% n-paraffins;

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- between about 2 and about 95 wt% branched paraffins wherein at least about 6 20% of all branch groups are monomethyl and wherein the ratio of terminal 7 monomethyl branching to internal monomethyl branching is at least about 1:1.5. 8 14. The synthetic fuel of claim 13 wherein the ratio of terminal monomethyl branching to 1 internal monomethyl branching is at least about 1:1. 2 15. The synthetic fuel of claim 13 wherein the n-paraffins are present in an amount of at least 1 about 10wt% and wherein the ratio of terminal monomethyl branching to internal 2 monomethyl branching is at least about 1.5:1. 3 16. The synthetic fuel of claim 13 wherein the n-paraffins are present in an amount of at least 1 about 10 wt% and wherein the ratio of terminal monomethyl branching to internal 2 monomethyl is at least about 2:1. 3 17. The synthetic fuel of claim 13 wherein the base fluid is a product of a Fischer-Tropsch 1 2 reaction. 18. The synthetic fuel of claim 17 wherein the Fischer-Tropsch reaction feed syngas comprises 1 2 10-65% N<sub>2</sub>. 19. A process for producing a synthetic fuel comprising the steps of: 1 producing a light Fischer-Tropsch liquid; (a) 2 distilling the light Fischer-Tropsch liquid to obtain a C8-C20+ product having C8-(b) 3  $C_{20+}$  hydrocarbons and FT oxygenates. 4
  - 5 (c) dehydrating all or a part of the FT oxygenates in the C<sub>8</sub>-C<sub>20+</sub> product while 6 retaining the olefin content of the C<sub>8</sub>-C<sub>20+</sub> product;
  - 7 (d) recovering the dehydrated product;
  - 8 (e) separating the aqueous and organic phases of the dehydrated product; and

- 9 (f) blending the organic phase of the dehydrated product into a transportation fuel.
- 1 20. The process of claim 19 wherein a  $C_{10}$ - $C_{20}$  product is obtained in step (b) and dehydrated in
- 2 step (c).
- 1 21. The process of claim 19 further comprising the step of (b<sub>1</sub>) vaporizing the C<sub>8</sub>-C<sub>20+</sub> product
- 2 before step (c) and after step (b).
- 1 22. The process of claim 19 wherein the dehydrated product from step (c) is in the gaseous state
- and step (d) further includes condensing the dehydrated product.
- 1 23. The process of claim 23 wherein the heat from condensing the dehydrated product is
- recycled to at least partially vaporize the  $C_8$ - $C_{20+}$  product in step  $(b_1)$ .
- 1 24. The process of claim 19 wherein the light Fischer-Tropsch liquid is produced from a feed
- 2 syngas having 10-65% N<sub>2</sub>.
- 1 25. The process of claim 24 wherein the feed syngas is produced by autothermal reformation in
- 2 the presence of air.
- 1 26. A synthetic transportation fuel comprising a non-hydroprocessed middle distillate fraction
- of a crude Fischer-Tropsch synthesis product comprising substantially no FT oxygenates.
- 1 27. The synthetic transportation fuel of claim 26 wherein the fuel has a cloud point of less than
- 2 or equal to 5°C.
- 1 28. The synthetic transportation fuel of claim 27 wherein the fuel contains less than 1wt%
- 2 aromatics.
- 1 29. The synthetic transportation fuel of claim 27 wherein the fuel contain less than or equal to
- 2 1ppm of nitrogen.
- 1 30. A transportation fuel produced by the process of claim 7.
- 1 31. A transportation fuel produced by the process of claim 19.

- 1 32. A blending stock for a transportation fuel produced by the process of claim 7.
- 1 33. A blending stock for a transportation fuel produced by the process of claim 19.
- 1 34. A synthetic transportation fuel consisting essentially of olefins and paraffins without
- 2 presence of hetero-atoms or additives wherein the transportation fuel has a lubricity
- measured in accordance with ASTM D-6079 of less than or equal to 0.45mm at 60°C.
- 1 35. A synthetic transportation fuel comprising paraffins and olefins derived from the product of
- 2 a Fischer-Tropsch synthesis and comprising no hetero-atoms or additives and having total
- insolubles of less than or equal to 1.5 mg/100 ml measured in accordance with ASTM D-
- 4 2274.
- 1 36. A synthetic transportation fuel comprising paraffins and olefins derived from the product of
- 2 a Fischer-Tropsch synthesis and containing no hetero-atoms having a lubricity measured in
- accordance with ASTM D-6079 of less than or equal to 0.45 mm at 60°C and a stability of
- 4 total insolubles of less than or equal to 1.5 mg/100 ml measured in accordance with ASTM
- 5 D-2274.